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Bubbly

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for DNB investigations The CFD Wall Boiling Model The wall surface is assumed to be split into two parts (A_1 , A_2) each under the influence of one phase. Fraction A_2 is influenced by the vapour bubbles formed on the wall and participates in the evaporation and quenching heat

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The description of boiling two-phase flow in CFD codes is commonly based on the two- fluid approach (Ishii, 1975), (Delhaye, 1981). In this

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approach, a set of local balance equations for mass,...

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Subcooled boiling in upward non-isothermal turbulent bubbly flow in tubes is numerically modeled using

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ANSYS-CFX 12 in this contribution.

The approach is based on the RPI wall boiling model developed by Kurul and Podowski. The interfacial non-drag forces are also investigated and included in the model.

CFD Modeling of Subcooled Boiling in

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continuous ($k = 1$) and dispersed bubbles ($k = 2$) and the mass

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This paper focuses on the Reynolds-averaged Navier-Stokes (RANS) approach as being the most reliable for simulation of realistic bubbly flows. New physical models developed within the NURESIM...

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boiling bubbly flow, CFD, DNB, fuel rod bundle - Begell ...

This paper focuses on the modelling and the numerical simulation with the NEPTUNE_CFD code of cavitation

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Phenomena and boiling bubbly flows. Compressible, unsteady, turbulent 3D two-phase flow is computed by the NEPTUNE_CFD solver, developed jointly by EDF R&D and CEA.

Modelling and computation of cavitation and boiling bubbly ...

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The PWR tests were considered in PSBT. This paper describes the use of three-dimensional computational fluid dynamics (CFD) to model the boiling two-phase flows in one of the 5-by-5 rod bundle tests. The commercial CFD software STAR-CCM+ v6.06 was used in this study. The rod bundle with all

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the spacers was modeled explicitly using unstructured computational grids.

CFD Modeling of Boiling Flow in PSBT
5 × 5 Bundle

The two-fluid model we use for our boiling bubbly flow calculations is

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constituted of the following six balance equations (e.g.,): (i) two mass balance equations: where is the time, denote the volumetric fraction of phase , its averaged density and velocity and is the interfacial mass transfer per unit volume and unit time; the phase index takes the values

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for the liquid phase and for the gas phase;

Modeling of Multisize Bubbly Flow and Application to the ...

The turbulent convection heat flux is calculated in the CFX model version (see Winterle, 2004) in much the

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Dr. Investigation
same way as for a pure liquid flow without boiling, but multiplied by the fraction of area unaffected by the bubbles, i.e.: $(2) Q C = (1 - A W) h C (T W - T L)$ Here $h C$ is the heat transfer coefficient which is written using the temperature wall function $T + (y +)$ known from Kader (1981) as

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(3) $h C = C P u T +$ where non-dimensional variables (indicated by superscript ...

CFD for subcooled flow boiling:

Simulation of DEBORA ...

CFD Modeling of Subcooled Boiling in Vertical Bubbly Flow Condition Using

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ANSYS CFX 12 <jats:p>Subcooled boiling in upward non-isothermal turbulent bubbly flow in tubes is numerically modeled using ANSYS-CFX 12 in this contribution. The approach is based on the RPI wall boiling model developed by Kurul and Podowski [1].

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For the bubbly flow analyzed during this study, the two-fluid model is comprised of two fields: liquid

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continuous ($k = 1$) and disperse d bubbles ($k = 2$) and the mass transfer across the interface is zero for adiabatic flows. Momentum conservation $t_k k k w D U X w$

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